## Results from ARMA Hydraulic Fracturing Code Comparison 2017 using Resfrac (code described in SPE-182593-MS)

### Benchmark Problem 6 (a,c)

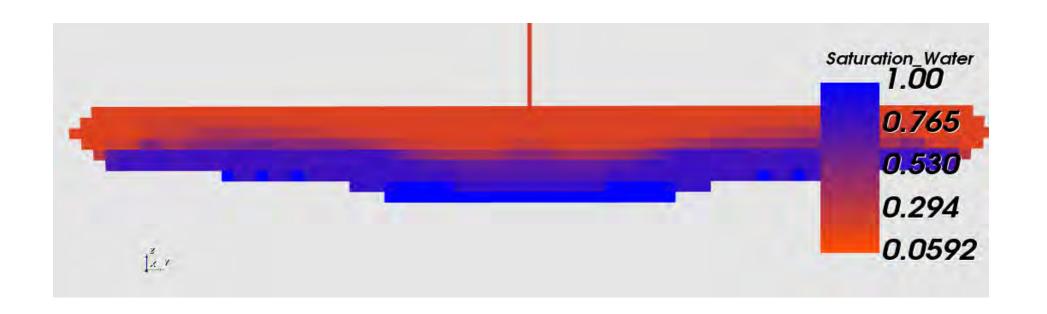
Note: We also did an "extended" 6c with 10 days of shut-in, followed by 90 days of production, to show the large changes that occurs *after* shut-in

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#### Resfrac SPE 182593-MS

- Full coupling between wellbore, reservoir, and hydraulic fracturing
- A true hydraulic fracturing simulator and a true reservoir simulator
- Ability to capture fracture closure, either with or without proppant, and smoothly transition between constitutive equations
- Thermal and compositional (three-phase)
- Proppant transport: gravitational settling, hindered settling, jamming, transition to Darcy flow, gravitational convection



#### Multiphase Forcheimer flow with gravity and non-Newtonian fluid Handles closure, with or without proppant

$$\begin{split} \frac{\Delta\Phi_p}{\Delta x} &= -\frac{q_{p,o}}{W} \left(\frac{12\mu_{p,s}}{E^3k_{rp,cro}}\right) + sgn(\Delta\Phi_p) \left(\frac{q_{p,o}}{WE}\right)^2 \beta_{cro}\beta_{rp,cro}\rho_{p,s} \\ \frac{\Delta\Phi_p}{\Delta x} &= -\left(\frac{q_{p,c}}{W}\right) \frac{1}{M_{p,cr} + M_{p,b}} + sgn(\Delta\Phi_p) \left(\frac{q_{p,c}}{WE}\right)^2 \rho_p \frac{M_{p,cr} + M_{p,b}}{\frac{M_{p,cr}}{\beta_{cr}\beta_{rp,cr}}} + \frac{M_{p,b}}{\beta_b\beta_{rp,b}} \\ \gamma_f &= \frac{E_{open}}{0.1(E_0 + E_{pr} + E_{res}) + E_{open}} \\ q_p &= \gamma_f q_{p,o} + (1 - \gamma_f) q_{p,c} \\ \Phi_p &= P_p - gz(\gamma_f \rho_p + (1 - \gamma_f)(C_{pr}\bar{\rho}_{pr} + (1 - C_{pr})\rho_p)) \\ \mu_a &= \frac{\mu_0}{1 + \frac{\mu_0}{K}(\dot{\gamma})^{1-n}} = \frac{\mu_0}{1 + (\frac{\dot{\gamma}}{\dot{\gamma}_{1/2}})^{1-n}} \end{split}$$

#### Modified power-law fluid (similar to an Ellis fluid)

$$\mu_a = \frac{\mu_0}{1 + \frac{\mu_0}{K} (\dot{\gamma})^{1-n}} = \frac{\mu_0}{1 + \left(\frac{\dot{\gamma}}{\gamma_{1/2}}\right)^{1-n}}$$

Behaves like a power-law fluid at high shear rate, but has a low-shear rate plateau.

Solute concentration and temperature related to rheological parameters.

Smoothly captures transition from Newtonian to non-Newtonian fluid as solute concentration increases.

Can set parameters to behave similar to power law.

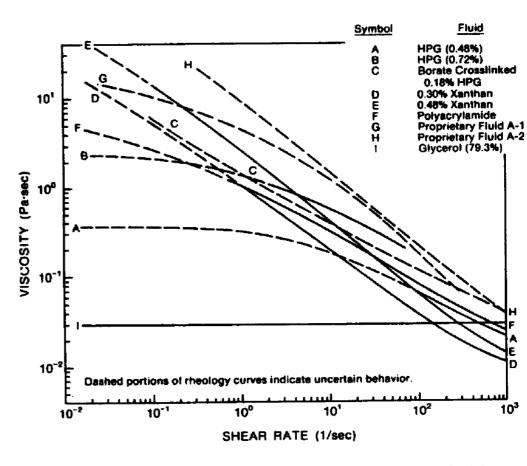
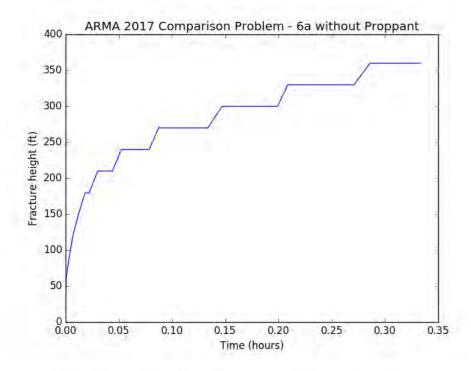


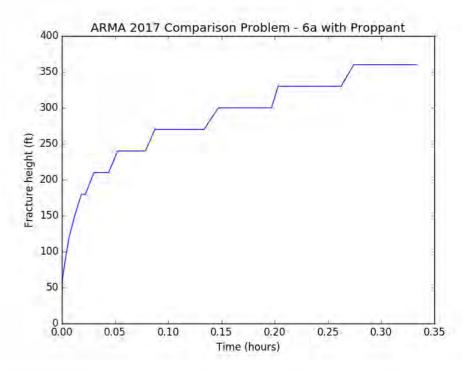
Figure 7. Rheological characterization of fluids.

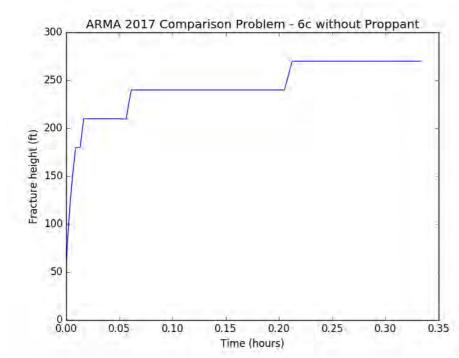
Kirkby and Rockefeller (1985)

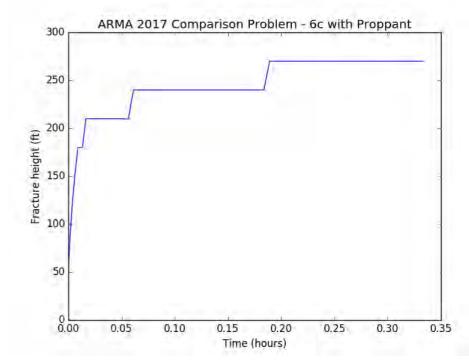
#### **Numerical Methods**

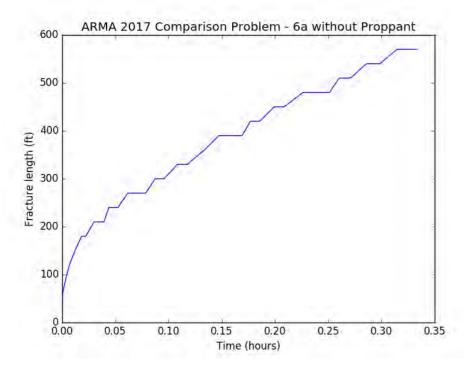
- Finite volume method for transport
- Boundary element method for mechanics
- Non-Newtonian flow in 6a (Newtonian fluid in 6c)
- In 6c, CO2 density calculation with Peng-Robinson equation of state, CO2 viscosity set constant to 15 cp
  - Injection rate:
    - "20 bpm" was assumed to refer to reservoir volume
    - For CO2, this was converted to 50 Mscf/min

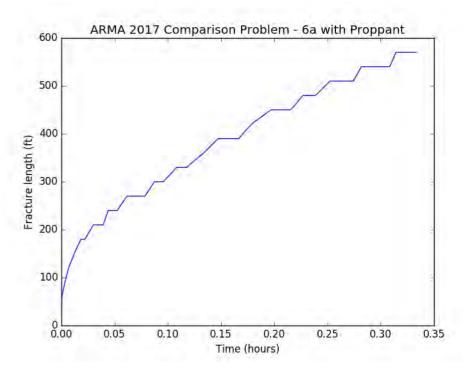


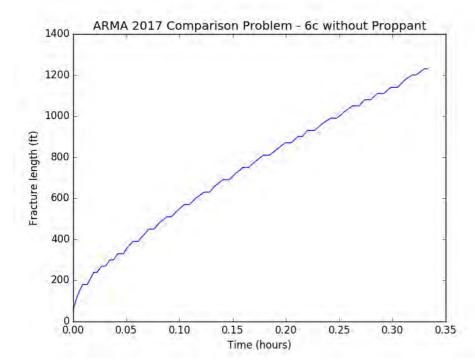


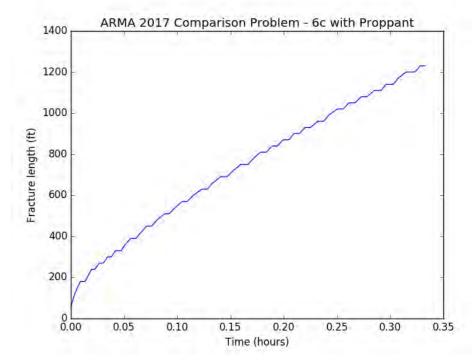


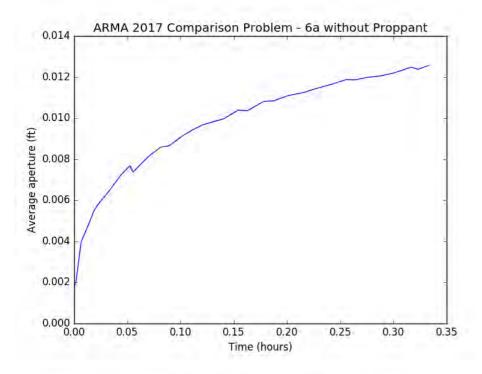


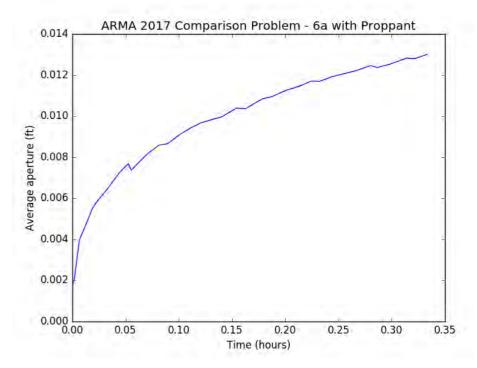


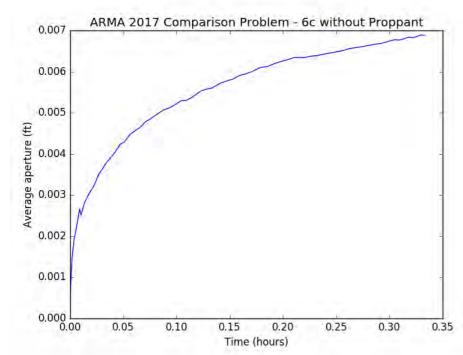


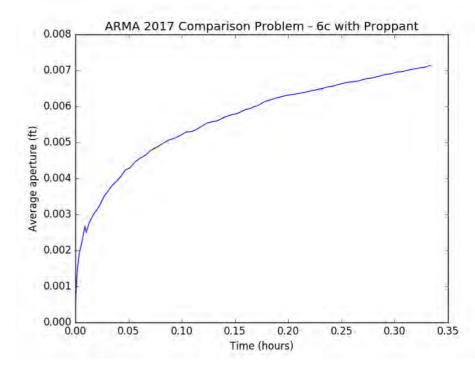


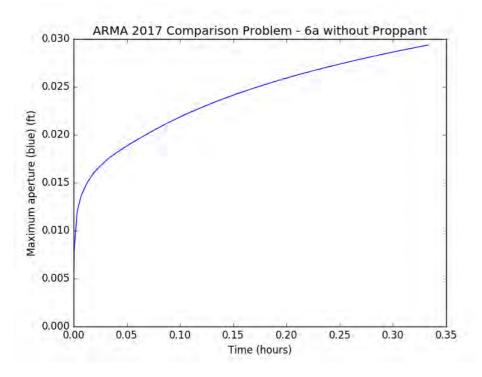


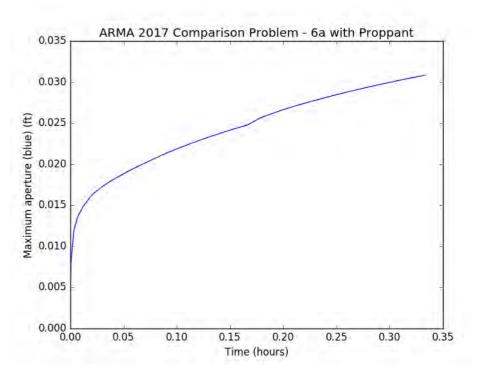


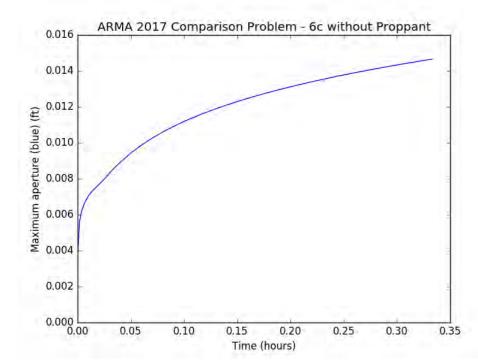


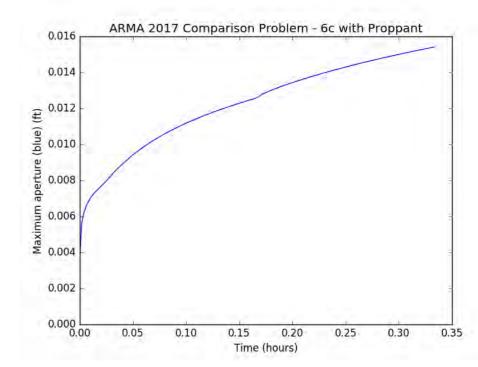


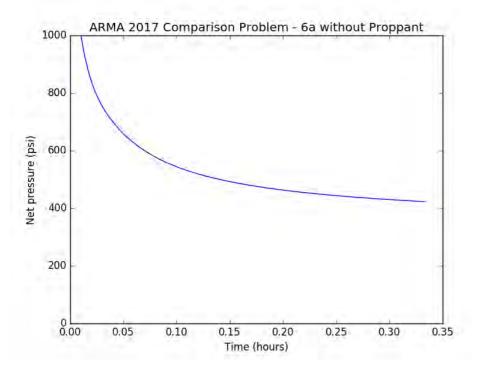


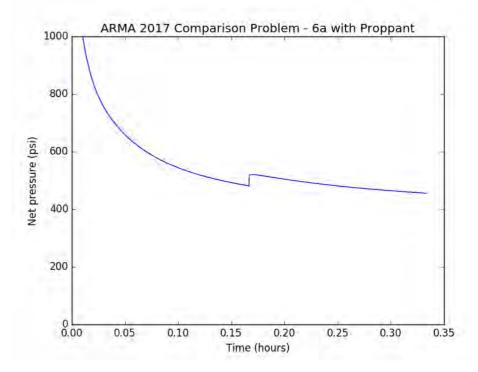


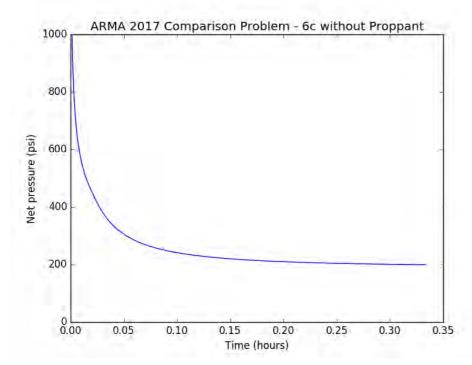


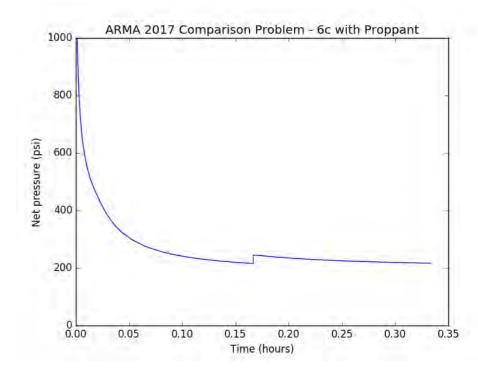


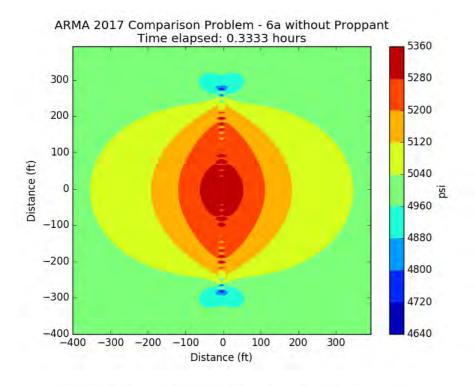


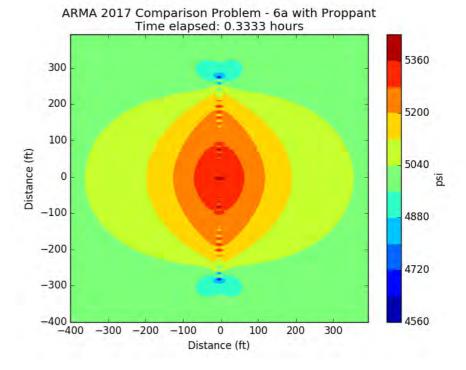


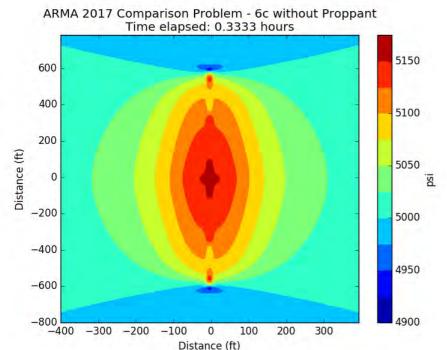


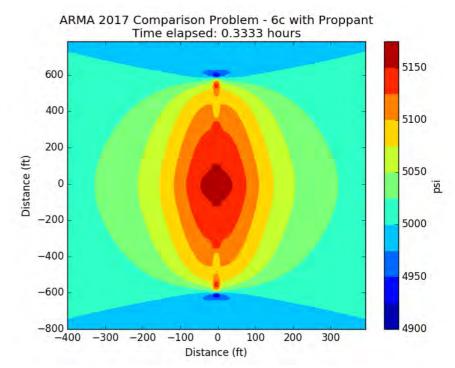


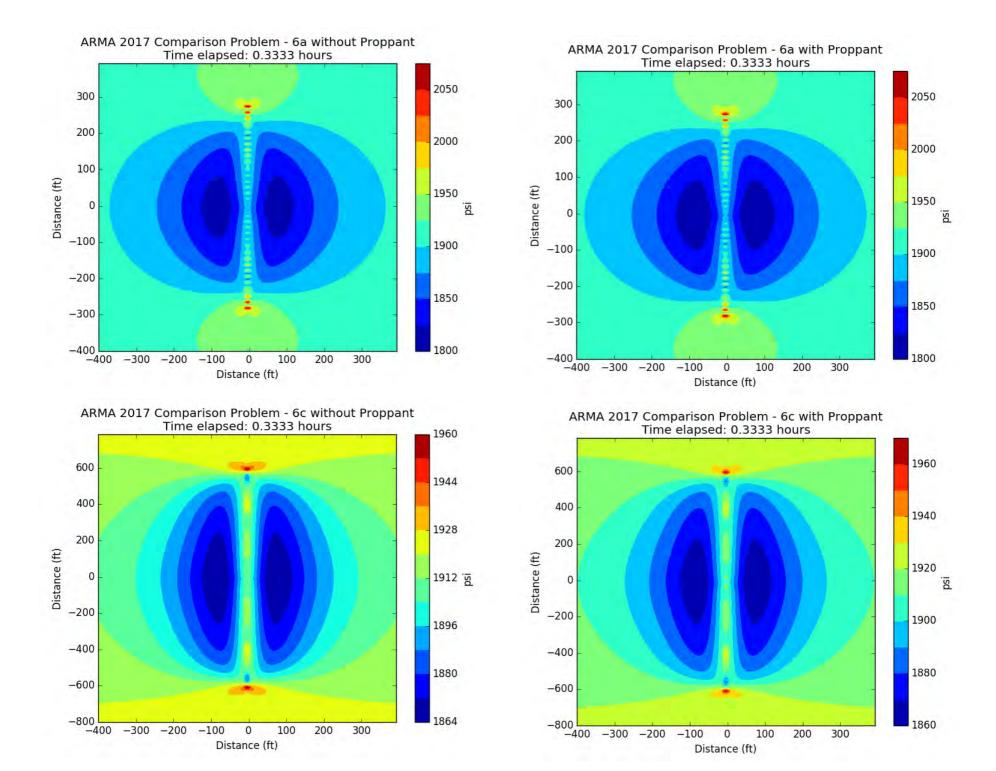


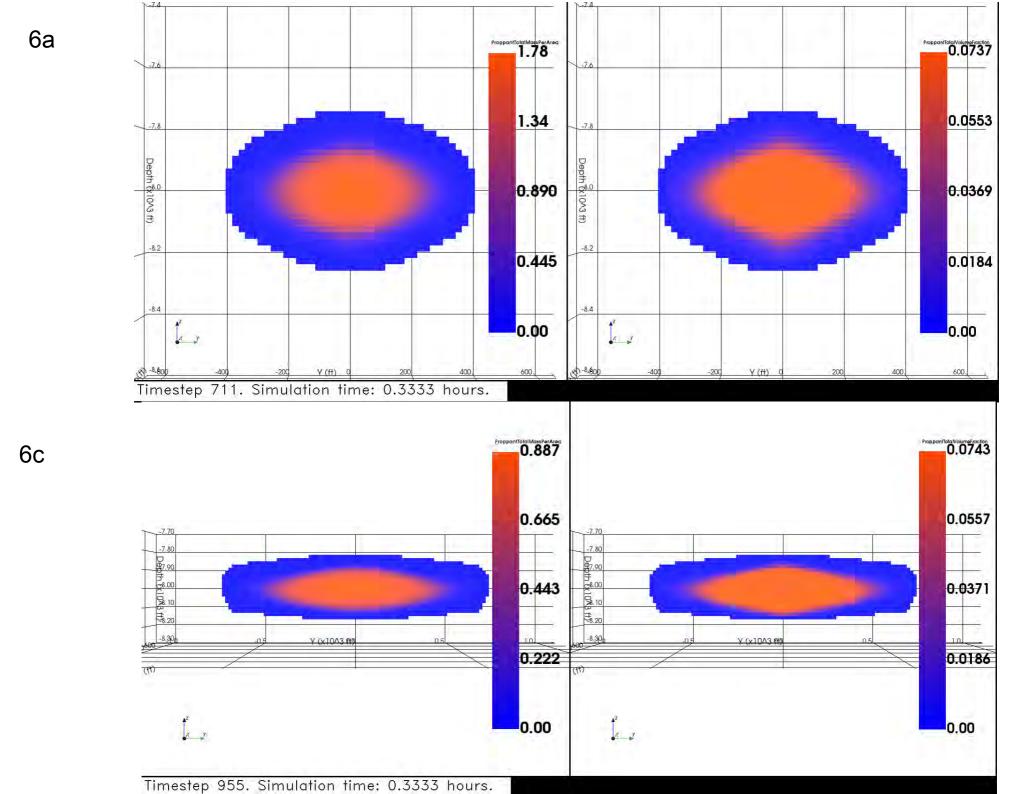


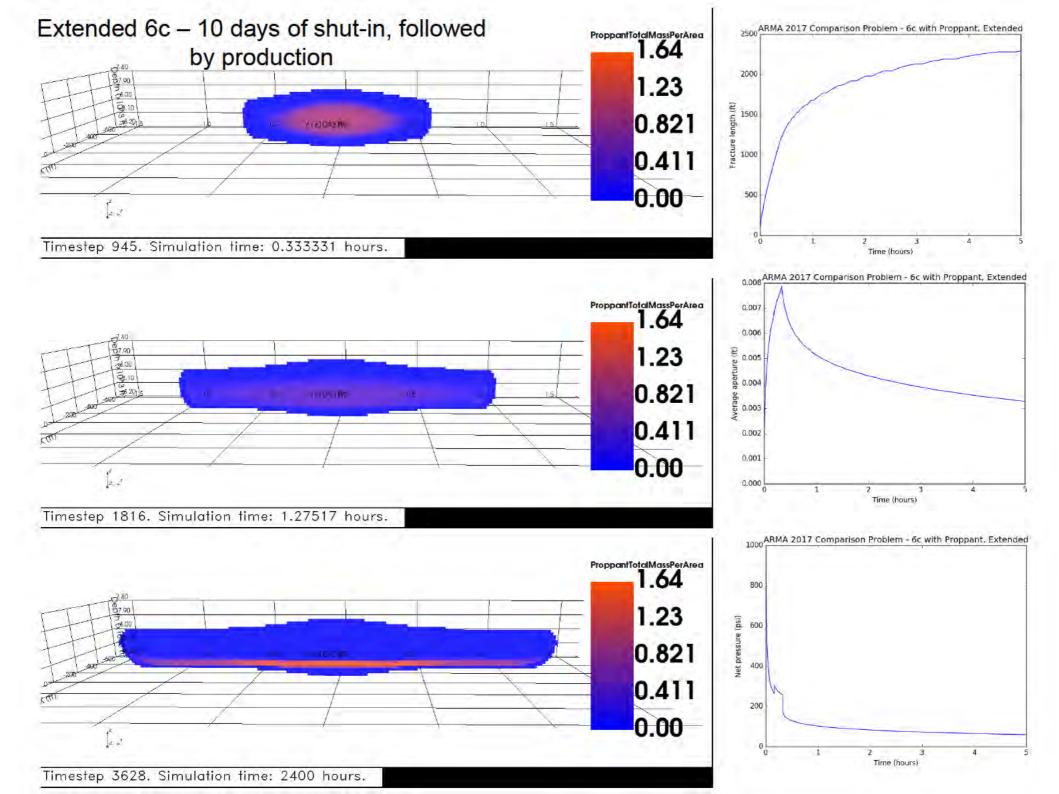




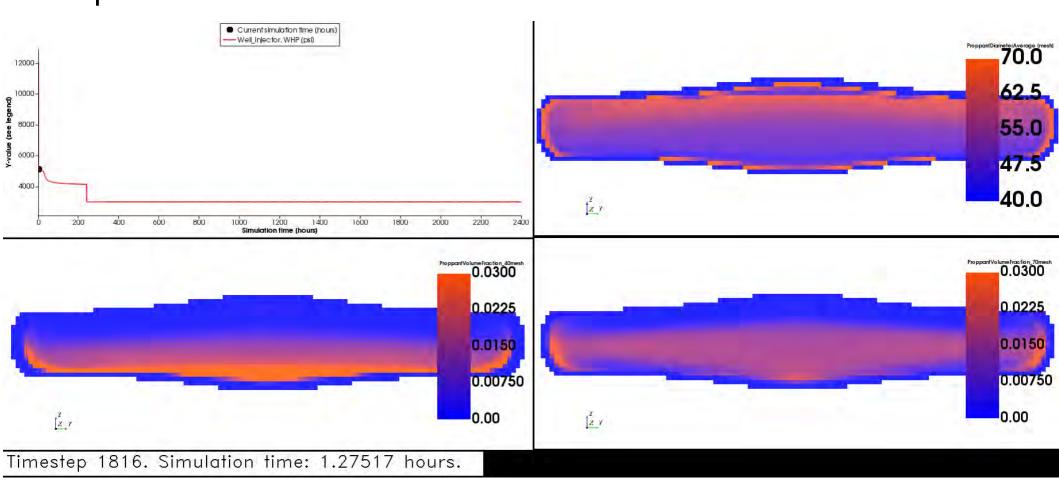




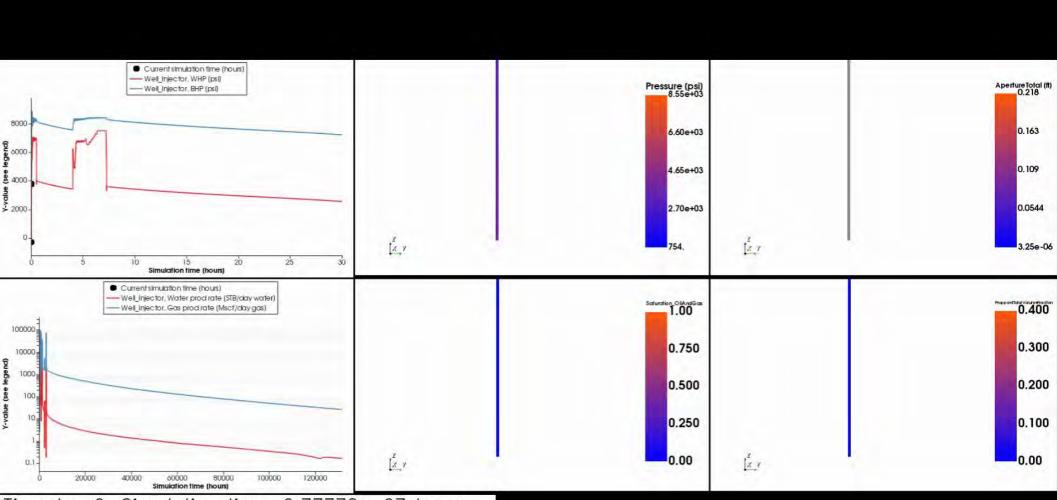




Mass balance is solved for four types of proppant: 40, 50, 60, and 70 mesh. This figure shows the gravitational segregation that occurs during shut-in (before closure) due to different settling velocities. Lower left is proppant volume fraction of 40 mesh. Lower right is proppant volume fraction of 70 mesh. Upper right is average proppant mesh as a function of position.



# Example of field-scale hydraulic fracturing and production



Timestep O. Simulation time: 2.77778e-07 hours.